

IN THE SPECIFICATION

Please replace the paragraph beginning at page 10, line 21, with the following rewritten paragraph:

Figure 2 is a schematic diagram of an apparatus for carrying out the second embodiment of the process according to the present invention. At the mixing site 21, the chlorosilane-containing gas stream 22 is introduced into the tubular reactor 23, whose inner walls are wetted with "another aqueous liquid" 32, such as tap water or deionized water. The walls of the tubular reactor 23 are cooled by the cooling agent 24. Upon entry into the tubular reactor 23, the velocity of the gas stream 22 decreases greatly. The treatment of the gas stream 22 with the steam originating from the other aqueous liquid 32 takes place in the tubular reactor 23, with formation of hydrogen chloride and primary hydrolysis products. The formation of secondary hydrolysis products takes place in the other aqueous liquid 32 which wets the wall of the equipment, resulting in a suspension. This suspension is separated from the purified gas stream 26 in the collecting container 25 and removed continuously or periodically as a hydrolyzate suspension 15. The purified gas stream 26 then passes through the scrubber 27 which can be charged, for example with water, and leaves the system as waste gas 28. Scrubber 27 may also be used for monitoring the content of residual silicon-containing compounds in the gas stream. To re-use the other aqueous liquid 32, the suspension can be recycled as a stream 29 until the concentration of the secondary hydrolysis products has reached a predetermined value. In addition, the circulation stream 29 can be treated to neutralize the hydrogen chloride formed by the hydrolysis of chlorosilanes with an aqueous alkaline liquid 31, which can be removed, for example, from the reservoir 30. If the other aqueous liquid 32 or the circulation stream 29 is rendered alkaline in this manner, largely soluble

silicon compounds result, thereby markedly reducing the tendency for deposits to form on tubular reactor 23 and collecting container 25.

Please replace the paragraph beginning at page 12, line 15, with the following rewritten paragraph:

Figure 3 is a schematic diagram of an apparatus for carrying out the third embodiment of the process of the present invention. At the mixing site 41, the chlorosilane-containing gas stream 42 and steam 43 are introduced into the tubular reactor 44, where the treatment of the chlorosilane-containing gas stream 42 with steam 43 takes place with formation of primary hydrolysis products. The tubular reactor 44 dips into the cooling container 45, whose inner walls are wetted with the “other aqueous liquid” 54. In addition, the walls of tubular reactor 44 can be cooled by means of a cooling agent 46. The flow rate of gas streams 42 and 43 greatly decreases upon entry into the cooling container 45. Steam 43 condenses in the interior of the cooling container 45, and the condensate is transported to the wetted equipment wall together with secondary hydrolysis products by means of a Stefan flow. The resulting suspension of secondary hydrolysis products, condensed steam 43 and other aqueous liquid 54 runs off the walls, is collected in the collecting container 47 and removed continuously or periodically. The purified residual gas 48 then passes through the scrubber 49, which may be charged, for example, with water, and leaves the system as waste gas 50. In addition, scrubber 49 may be used to ~~monitoring~~ monitor the residual content of silicon-containing compounds in the gas stream. In the third embodiment of the process of the present invention, it is generally not necessary to remove hydrogen chloride from the waste gas 50. In order to minimize use of the “other aqueous liquid” 54, the suspension may be recycled as

stream 51 until the concentration of the secondary hydrolysis products has reached a predetermined value. In addition, the circulation stream 51 may be treated with an aqueous alkaline liquid 53, for example, from the reservoir 52, to neutralize the hydrogen chloride formed by hydrolysis of chlorosilanes. If the “other aqueous liquid” 54 or the circulation stream 51 is rendered alkaline in this manner, largely soluble silicon compounds result, thereby markedly reducing the tendency deposits to form on cooling containers 45 and collecting container 47.